

This Page Is Inserted by IFW Operations
and is not a part of the Official Record

BEST AVAILABLE IMAGES

Defective images within this document are accurate representations of the original documents submitted by the applicant.

Defects in the images may include (but are not limited to):

- BLACK BORDERS
- TEXT CUT OFF AT TOP, BOTTOM OR SIDES
- FADED TEXT
- ILLEGIBLE TEXT
- SKEWED/SLANTED IMAGES
- COLORED PHOTOS
- BLACK OR VERY BLACK AND WHITE DARK PHOTOS
- GRAY SCALE DOCUMENTS

IMAGES ARE BEST AVAILABLE COPY.

**As rescanning documents *will not* correct images,
please do not report the images to the
Image Problem Mailbox.**

Attorney Docket: 817LR/50045
PATENT

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

Applicant: ROBERT M. STEWART ET AL.

Serial No.: Not Yet Assigned

Filed: August 29, 2001

Title: PROCESS AND APPARATUS FOR COAGULATING AND DRYING
LATEX



CLAIM FOR PRIORITY UNDER 35 U.S.C. §119

Box PATENT APPLICATION

Commissioner for Patents
Washington, D.C. 20231


Sir:

The benefit of the filing date of prior foreign application No. PI 2000 3975, filed in Malaysia on August 29, 2000, is hereby requested and the right of priority under 35 U.S.C. §119 is hereby claimed.

In support of this claim, filed herewith is a certified copy of the original foreign application.

Respectfully submitted,

August 29, 2001



James F. McKeown
Registration No. 25,406

CROWELL & MORING, LLP
P.O. Box 14300
Washington, DC 20044-4300
Telephone No.: (202) 624-2500
Facsimile No.: (202) 628-5116



KEMENTERIAN PERDAGANGAN DALAM NEGERI
DAN HAL EHWAL PENGGUNA MALAYSIA,
BAHAGIAN HARTA INTELEK,
TINGKAT 27, 30 DAN 32,
MENARA DAYABUMI,
JALAN SULTAN HISHAMUDDIN,
50623 KUALA LUMPUR

*Ministry of Domestic Trade and Consumer Affairs Malaysia,
Intellectual Property Division*

Telefon: 03-2741000
Fax: 2741332

Fail Tuan:

Fail Kita:

Tarikh:

To:



LEE TATT BOON

Skrine & Co.

8 - 10 th Floors, Wisma UOA Damansara,
50, Jalan Dungun, Damansara Height,
50490 Kuala Lumpur,
MALAYSIA.

PATENT APPLICATION NO: PI 2000 3975

This is to certify that annexed hereto is a true
copy from the records of the Registry of Trade Marks
and Patents, Malaysia of the application as originally
filed which is identified therein.

By authority of the
REGISTRAR OF PATENTS

ABDUL RAHMAN RAMLI
(CERTIFYING OFFICER)
24 May 2001



KEMENTERIAN PERDAGANGAN DALAM NEGERI
DAN HAL EHWAL PENGGUNA MALAYSIA
BAHAGIAN HARTA INTELEK,
TINGKAT 27 & 32,
MENARA DAYABUMI,
JALAN SULTAN HISHAMUDDIN,
50654 KUALA LUMPUR.
*Ministry of Domestic Trade and Consumer Affairs Malaysia
Intellectual Property Division.*


Telefon: 03-22742100
Fax : 03-22741332

CERTIFICATE OF FILING

APPLICANT : LINATEX RUBBER PRODUCTS SDN BHD
APPLICATION NO : PI 20003975
REQUEST RECEIVED ON : 29/08/2000
FILING DATE : 29/08/2000
AGENT'S/APPLICANT'S FILE REF. : LTB/YTL/SH/2003726.6

Please find attached, a copy of the Request Form relating to the above application, with the filing date and application number marked thereon in accordance with Regulation 25(1).

Date : 19/09/2000


.....
(HASNON BT. ALANG MOHD RASHID)
for Registrar of Patents

To : LEE TATT BOON
C/O M/S SKRINE & CO.,
50-8-1, 8TH FLOOR, WISMA UOA DAMANSARA, 50,
JALAN DUNGUN, DAMANSARA HEIGHTS,
50490 KUALA LUMPUR
MALAYSIA

A PROCESS AND APPARATUS FOR COAGULATING AND DRYING LATEX

5 The present invention relates to a process and apparatus for the continuous coagulation and drying of a rubber latex. In the specification the term "rubber latex" includes both a natural rubber latex and synthetic rubber latices.

10 There has previously been proposed and developed a process in which a rubber latex is fed through a coagulator in which the temperature of the latex is raised sufficiently to cause the latex to coagulate to form coagulated rubber. The coagulated rubber is then fed through a dryer which reduces the moisture content of the coagulated rubber to an acceptable level.

15 In the above-mentioned conventional process, the coagulation of the rubber latex can take several hours, and the drying process can take more than 15 hours.

20 It is an aim of the invention to provide a process and apparatus for the continuous coagulation and drying of rubber latex in which the above-mentioned coagulation and drying times are reduced and there is a more precise control of the coagulation and drying process.

25 According to one aspect of the invention there is provided a process for the continuous coagulation and drying of rubber latex, the process comprising passing a stream of the latex through a coagulator to form coagulated rubber, introducing the coagulated rubber stream from the coagulator into a dryer downstream of the coagulator, and passing the coagulated rubber through the

dryer to dry the rubber, in which the latex stream in the coagulator is heated by a combination of microwave energy and hot air to cause the latex to coagulate.

5 The coagulation temperature may be in the range from 30°C to 90°C, and preferably the latex stream entering the coagulator may have a thickness in the range from 1.0mm to 15.0mm.

10 The coagulated rubber in the dryer may also be heated by a combination of microwave energy and hot air to dry the rubber, and the rubber may be dried to have a moisture content of less than 1.5%.

15 The process may also include stretching the coagulated rubber stream as it passes between the coagulator and the dryer, and preferably this coagulated rubber stream is stretched by increasing the speed at which the stream is conveyed to the dryer.

20 According to another aspect of the invention there is provided an apparatus for the continuous coagulation and drying of rubber latex, the apparatus comprising a coagulator, first feeding means to pass a stream of latex through the coagulator to form coagulated rubber, a primary heating means operable to provide a combination of microwave energy and hot air to coagulate the latex stream passing through the coagulator, a dryer to receive the coagulated rubber stream from the coagulator, second feeding means to pass the coagulated rubber stream through the dryer, and secondary heating means to dry the coagulated rubber passing through the dryer.

25

The secondary heating means may also be operable to provide a combination of microwave energy and hot air to dry the rubber.

5 The apparatus may also include a stretch unit to stretch the coagulated rubber stream leaving the coagulator before it enters the dryer, and preferably the first and second feeding means are conveyor belts.

10 An embodiment of the invention will now be described by way of example with reference to the accompanying illustrative drawings in which:-

Figure 1 is a side elevation of a plant for coagulating and drying rubber latex, and

Figure 2 is a plan view of the plant of Figure 1.

15 Referring to the drawings, the material from which the rubber is formed is a fully compounded natural rubber latex containing a chemical dispersion of sulphur, zinc oxide, accelerators, antioxidants, antidegradents and a heat sensitising agent. This latex is prepared in a mixing and metering unit (2) and the prepared latex is
20 fed through a feed pipe (4) and a dispenser (6) onto an endless conveyor belt (8) which is coated with polytetrafluoroethylene (PTFE) to prevent coagulated rubber from sticking to the belt. The feed of the latex onto the belt (8) is controlled to provide a uniform thickness of latex in the range from 1.0mm to 15.0mm
25 across the full width of the conveyor belt (8).

The belt (8) feeds the latex through a coagulator (10)

which produces a combination of microwave energy and a supply of hot air to raise the temperature of the latex to a level to cause the latex to coagulate. The coagulation temperature is normally in the range from 30°C to 90°C depending on the specific formulation of the latex used.

The coagulator is 12.5 metres in length which includes a 1 metre long latex feed system at the inlet of the coagulator (10). The endless belt (8) extends around a drive pulley and a driven pulley located at the inlet and outlet of the coagulator (10) so that the belt (8) returns through the coagulator (10). The belt is dimensioned to support a latex product width of 1.25 metres and the belt is located up to 1.0 metres from the floor of the coagulator (10). The belt specification and the support structure are designed so that the belt is flat and level over its complete length within plus or minus 0.1mm. The belt drive system is designed to ensure correct and consistent tracking of the belt (8) and provision is made to allow any inclination of the belt from the horizontal to be adjusted on site.

The invention is not restricted to plant components of any specific size. For example, the width of the apparatus can be varied according to the required width of the product. The length of the coagulator (10) is determined by the required flow rate of the latex; the higher the required latex flow rate, the longer the coagulator (10) has to be.

A liquid catch tray and a scraper are fitted around the drive pulley to collect and remove uncoagulated latex

from the belt. A lightweight roller is fitted at the outlet of the coagulator to assist in removal of uncoagulated latex from the belt. This roller is designed for easy removal to allow access for cleaning the catch tray and scraper. A belt cleaning unit is provided, and this unit is designed so that the belt (8) can be replaced without removing any other part of the apparatus. An illuminated viewing port is fitted to the coagulator so that the coagulation process can be examined.

A stretch unit (12) consists of an endless conveyor belt (14) coated with PTFE. The belt (14) is dimensioned to accommodate a product width of 1.25 metres. The belt (14) travels around a drive pulley and a driven pulley which are designed to ensure correct and consistent tracking of the belt. The invention is not restricted to plant components for handling a specific product width.

A pneumatically-operated nip roller is located above the driven return roller of the belt (14).

In operation, the belt (14) of the stretch unit is driven at a higher speed than the belt (8) of the coagulator (10) so as to increase the speed at which the coagulated rubber leaving the coagulator (10) is conveyed. This speed increase of the coagulated rubber stretches the rubber so as to increase the surface area of the rubber thereby reducing the time the rubber takes to dry.

The stretched rubber is then conveyed into a drying unit (16) containing three endless conveyor belts (18), (20) and (22) located one above the other. All three belts

have an open mesh to improve the drying rate of the rubber, and are coated with PTFE. The three belts are dimensioned to accommodate a product width of 1.25 metres, and the drying unit (16) is designed so that all three belts can be replaced without having to remove any other part of the drying unit.

The three belts each pass around their associated drive pulley and driven pulley, and the belt drive system is designed to ensure correct and consistent tracking of the belts.

The coagulated rubber leaving the stretch unit belt (14) passes onto the inlet of the upper drying unit belt (18) which travels in a clockwise direction to deposit rubber from its outlet end onto the inlet end of the intermediate belt (20) which travels in an anti-clockwise direction to deposit the rubber from its own outlet end onto the inlet end of the lower belt (22) which travels in a clockwise direction. This lower belt 22 conveys the coagulated rubber to the outlet of the drying unit (16).

The drying unit (16) uses a combination of microwave energy and hot air in the belt triple-pass system to reduce the final moisture content of the coagulated rubber to less than 1.5%.

The drying belt (16) in this example of the invention is three pass, i.e. the coagulated rubber is passed in sequence over three belts located in series. The drying unit (16) could however have any odd number of belts in series. The important feature is that the coagulated rubber is retained in the drying unit sufficiently long

to dry the rubber to a required level.

The dispenser (6) is a fully welded construction using stainless steel to ensure that there is no rusting that can lead to contamination of the product.

5 To ensure the dispenser is easy to clean all surfaces that come into contact with the latex are coated with polytetrafluoroethylene (PTFE) (Teflon).

10 The dispenser (6) is set level across the width of the belt (8) on to which the latex is deposited. This has to be set up very accurately using a built-in levelling system, to ensure that, together with the constant flow delivered via a metering system, the correct thickness of product is achieved.

15 The dispenser is moved from the standby position to the ready position using a small compressed air cylinder.

20 The design of the dispenser ensures that there are minimum restrictions in the system to provide an even flow to the product. This design, along with the flow and levelness of the system, is essential in giving accurate control to the thickness of the product.

25 Microwave chokes are provided at both ends of the above units. These chokes are designed for a maximum product thickness of 150mm but they are adjustable to suit a minimum product thickness of 1.5mm. Microwave leakage detectors are fitted at both ends of each of the above units.

The recirculating hot air system of the coagulator (10) and the drying unit (16) is designed for automatic control at any temperature from ambient up to a maximum temperature of 100°C, and the warm-up time from ambient to maximum temperature will not exceed 15 minutes.

Should the system be capable of generating temperatures in excess of the required maximum then interlocks must be provided to prevent this taking place. The control of the recirculating hot air will be carried out by use of a variable speed fan. Distribution of airflow into the units must be such that it does not cause either the leading edge of the product to fall back upon itself or, specifically and of the upmost importance in the coagulator (10), a wave effect on the product surface.

All units will be lagged such that the external temperature of any part of the units does not exceed 40°C. All units will be fitted with access doors to facilitate access for cleaning. These doors will be interlocked to shut down the unit in the event of entering during operation, and to prevent the unit being started up unless all the doors are in position and locked. The interlocks will be wired for no auto-restart. In this embodiment of the invention the metal used will be stainless steel, grade 304L. Product sensors are fitted and linked to the microwave power system to provide automatic power adjustment during the start-up and shutdown, or any other breaks in production.

The microwave heating process in the coagulator (10) has the following advantages:-

(1) the temperature of the latex can be controlled with

great accuracy,

(2) the coagulation process time is significantly reduced as the microwave energy heats the water containing the rubber from within. In previously known processes the coagulation time could be up to several hours whereas in this process the coagulation time is less than five minutes, and

(3) this process is energy-efficient when compared to previously known processes.

The microwave heating process in the drying unit (16) has similar advantages to that of the coagulator (10). The drying time in the drying unit (16) is less than 30 minutes compared to more than 15 hours in a previously known process.

CLAIMS

1. A process for the continuous coagulation and drying of rubber latex, the process comprising passing a stream of the latex through a coagulator to form coagulated rubber, introducing the coagulated rubber stream from the coagulator into a dryer downstream of the coagulator, and passing the coagulated rubber through the dryer to dry the rubber, in which the latex stream in the coagulator is heated by a combination of microwave energy and hot air to cause the latex to coagulate.
5
2. A process as claimed in claim 1 in which the coagulation temperature is in the range from 30°C to 90°C.
10
3. A process as claimed in claim 1 or claim 2 in which the latex stream entering the coagulator has a thickness in the range from 1.0mm to 15.0mm.
4. A process as claimed in any preceding claim in which the coagulated rubber in the dryer is heated by a combination of microwave energy and hot air to dry the rubber.
15
5. A process as claimed in claim 4 in which the rubber is dried to a moisture content of less than 1.5%.
20
6. A process as claimed in any preceding claim in which the latex stream speeds, rubber temperatures and microwave energy consumption are computer-controlled.
7. A process as claimed in any preceding claim including stretching the coagulated rubber stream as it
25

passes between the coagulator and the dryer.

8. A process as claimed in claim 7 in which the coagulated rubber stream is stretched by increasing the speed at which it is conveyed to the dryer.

5 9. An apparatus for the continuous coagulation and drying of rubber latex, the apparatus comprising a coagulator, first feeding means to pass a stream of latex through the coagulator to form coagulated rubber, a
10 primary heating means operable to provide a combination of microwave energy and hot air to coagulate the latex stream passing through the coagulator, a dryer to receive the coagulated rubber stream from the coagulator, second
15 feeding means to pass the coagulated latex stream through the dryer, and secondary heating means to dry the coagulated rubber passing through the dryer.

10. An apparatus as claimed in claim 9 in which the primary heating means is operable to provide a coagulation temperature in the range from 30°C to 90°C.

20 11. An apparatus as claimed in claim 9 or claim 10 in which the first feeding means is a conveyor belt.

12. An apparatus as claimed in claim 11 in which the conveyor belt is coated with polytetrafluoroethylene (PTFE).

25 13. An apparatus as claimed in any one of claims 9 to 12 in which the secondary heating means is operable to provide a combination of microwave energy and hot air to dry the rubber.

14. An apparatus as claimed in any one of claims 9 to 13 in which the second feeding means is a conveyor belt.

5 15. An apparatus as claimed in claim 14 in which the second feeding means is a plurality of conveyor belts arranged so that the coagulated rubber is passed from one belt to the other.

10 16. An apparatus as claimed in claim 14 or claim 15 in which the or each belt is coated with polytetrafluoroethylene (PTFE).

17. An apparatus as claimed in any one of claims 9 to 16 including a stretch unit to stretch the coagulated rubber stream leaving the coagulator for the dryer.

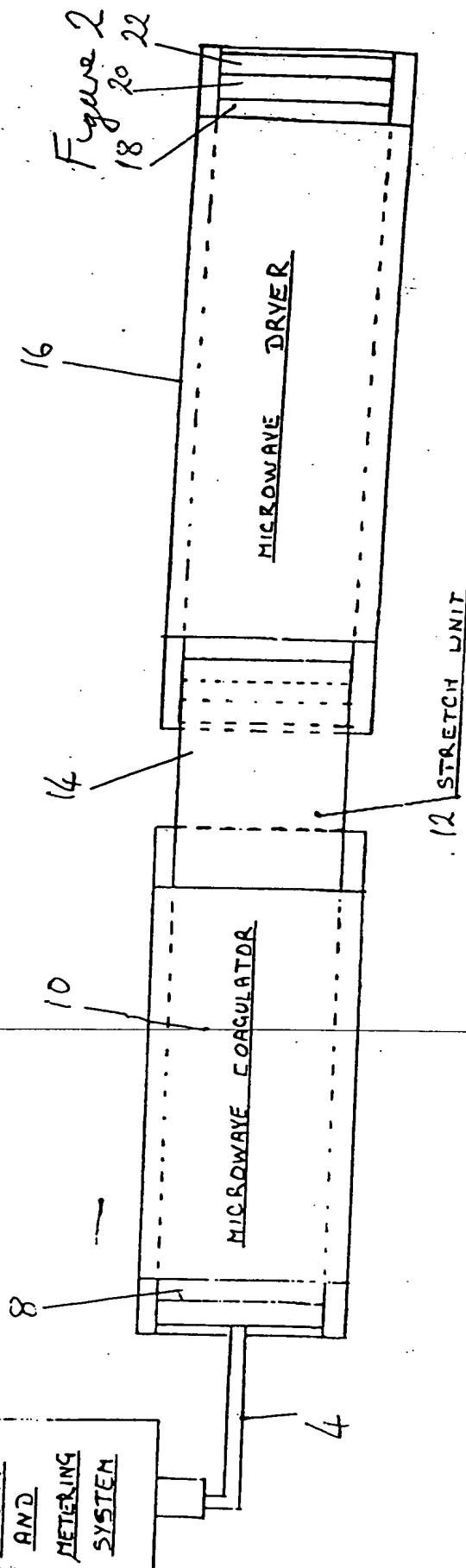
15 18. An apparatus as claimed in claim 17 in which the stretch unit is operable to increase the speed at which the coagulated rubber stream leaves the coagulator and enters the dryer.

20 19. An apparatus as claimed in claim 17 or claim 18 in which the stretch unit comprises a conveyor belt to receive the coagulated rubber leaving the coagulator and to pass the coagulated rubber to the input of the dryer.

20. An apparatus as claimed in claim 19 in which the belt is coated with polytetrafluoroethylene (PTFE).

25 21. A process for the continuous coagulation and drying of rubber latex substantially as herein described with reference to the accompanying drawings.

22. An apparatus for the continuous coagulation and drying of rubber latex substantially as herein described and shown in the accompanying drawings.



ABSTRACT**A PROCESS AND APPARATUS FOR COAGULATING AND DRYING LATEX**

A process for the continuous coagulation and drying of rubber latex includes feeding the latex onto an endless conveyor belt (8) which feeds the latex through a coagulator (10). A combination of microwave energy and hot air raises the temperature of the latex causing it to coagulate in a coagulation time of less than five minutes. The coagulated rubber from the coagulator (10) is fed onto a conveyor belt (14) of a stretch unit (12) which stretches the rubber by increasing its speed of travel. The stretched rubber is then conveyed onto the upper belt (18) of a drying unit (16). The drying rubber is passed from the upper belt (18) onto an intermediate belt (20) and then on to a lower belt (22) before leaving the drying unit (16). A combination of microwave energy and hot air in the drying unit (16) is used to dry the rubber to a moisture content of less than 1.5%.